CLAIMS

(I)

wherein:

T is -F, C_1 - C_3 perfluoroalkyl, -CH₂OH, -CH₂NH₂, -CHO; T'= T with the proviso that when T is F or C_1 - C_3 perfluoroalkyl, T' is -CH₂OH, -CH₂NH₂, -CHO;

X', X', equal to or different from each other, are -F or $-CF_3$;

 R_f is selected from:

-(C₂F₄O)_m(CF₂CF(CF₃)O)_n(CF₂O)_p(CF(CF₃)O)_qwherein the sum n+m+p+q ranges from 2 to 200,
the (p+q)/(m+n+p+q) ratio is lower than or equal to
10:100, preferably comprised between 0.5:100 and 4:100,
the n/m ratio ranges from 0.2 to 6, preferably from 0.5
to 3; m, n, p, q are equal to or different from each
other and when m, n range from 1 to 100, preferably from
1 to 80, then p, q range from 0 to 80, preferably from 0
to 50; the units with n, m, p, q indexes being
statistically distributed along the chain;

- -(CF₂CF₂CF₂O)_r- wherein r ranges from 2 to 200,
- -(CF(CF₃)CF₂O)_s- wherein s ranges from 2 to 200, comprising the following steps:

(AF 2657/031.EST)

terit i titt medeller i

A) preparation of perfluoropolyethers of formula $T'' - CFX' - O - R_f - CFX - COF$ (II)

wherein T'' is -COF, -F, C_1 - C_3 perfluoroalkyl, X, X', R_f are as above, by reduction of the corresponding perfluoropolyethers containing peroxidic bonds, with gaseous hydrogen in the presence of a catalyst formed by metals of the VIII group supported on metal fluorides, at a temperature from 20°C to 140°C, and at a pressure between 1 and 50 atm;

- B) treatment of the formula (II) compounds with inorganic chlorides, preferably CaCl₂, by heating at a temperature in the range 100°-150°C obtaining perfluoropolyethers having acylchloride -COCl end groups;
- B') treatment of the formula (II) acylfluoride or of the corresponding ester or of the corresponding acylchloride with gaseous ammonia, obtaining the corresponding amide, subsequently dehydrated preferably with P_2O_5 , at a temperature in the range $150^{\circ}-200^{\circ}C$, preferably at $170^{\circ}C$, with the obtainment of perfluoropolyethers with nitrile -CN end groups;
- c) reduction of the perfluoropolyethers with acylchloride end groups, obtained in step B), or with nitrile end groups, obtained in step B'), of formula

(IIa):

$$T'''-CFX'-O-R_f-CFX-T'''$$
 (IIa)

wherein:

T'''' = -F, C_1-C_3 perfluoroalkyl, -CN, -COCl, T''''' = T'''' with the proviso that when T'''' is -F or C_1-C_3 perfluoroalkyl, T''''' is -CN, -COCl, with gaseous hydrogen in the presence of a catalyst constituted by metals of the VIII group selected from Pd, Rh, Ru, supported on solid metal fluorides, at a temperature from 20°C to 150°C, preferably from 80°C to 120°C and at a pressure between 1 and 50 atm, preferably between 1 and 10 atm, optionally in the presence of inert solvents.

- 2. A process according to claim 1, wherein $R_{\rm f}$ is selected from the following structures:
 - $-(CF_2CF_2O)_m (CF_2O)_p ,$
 - $(CF_2CF(CF_3)O)_n$ $(CF_2O)_p$ $(CF(CF_3)O)_q$.
- 3. A process according to claims 1-2, wherein the metal fluoride of step C) is selected from the group formed by CaF_2 , BaF_2 , MgF_2 , AlF_3 , preferably CaF_2 .
- 4. A process according to claims 1-3, wherein the concentration of the VIII group metal on the metal fluoride of the catalyst of step C) is comprised beteen 0.1% and 10% with respect to the total weight of the catalyst, prefe-

rably between 1% and 2% by weight.